

Application No. 10/813,250
Reply to Advisory Action of 07/17/2008

Page 2

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Amendments to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application.

Listing of Claims:

Claims 1-2 (previously canceled)

Claim 3 (previously amended): The process of claim 28 wherein the sulfur-oxidated compounds are selected from the group consisting of sulfoxides and sulfones.

Claim 4 (previously amended): The process of claim 28 wherein the adsorbent is selected from the group consisting essentially of activated charcoal, hydrotalcite, ion exchange resin, zeolites, silica-alumina, and silica gel.

Claim 5 (previously amended): The process of claim 28 wherein the adsorbent having adsorbed sulfur-oxidated compounds contains from about 0.2 to about 2 weight percent sulfur-oxidated compounds.

Claim 6 (previously amended): The process of claim 28 wherein the contacting in step (a) is conducted at a temperature from about 25°C (77°F) to about 125°C (257°F) and a pressure from about 1240 kPa (165 psig) to about 1825 kPa (250 psig).

Claim 7 (previously amended): The process of claim 28 wherein the desorbent in step (c) is introduced at a temperature from about 43°C (110°F) to about 125°C (257°F).

Claim 8 (previously amended): The process of claim 28 wherein the desorbent comprises pentane, hexane, benzene, toluene, or xylene.

Claims 9-10 (previously canceled)

Claim 11 (previously amended): The process of claim 28 wherein the hydrocarbonaceous stream comprises diesel boiling range hydrocarbons.

Claims 12-22 (previously canceled)

Claims 23-24 (canceled herein)

Application No. 10/813,250
Reply to Advisory Action of 07/17/2008

Page 3

Claims 25-26 (previously canceled)

Claim 27 (canceled herein)

Claim 28 (previously amended): A process for the removal of sulfur-oxidated compounds from a hydrocarbonaceous stream containing sulfur-oxidated compounds wherein the process comprises:

- (a) contacting a hydrocarbonaceous stream containing sulfur-oxidated compounds with an adsorbent which selectively adsorbs sulfur-oxidated compounds to produce an adsorbent having adsorbed sulfur-oxidated compounds;
- (b) contacting the adsorbent having adsorbed sulfur-oxidated compounds with a desorbent to produce a desorbent containing sulfur-oxidated compounds and an adsorbent having a reduced content of sulfur-oxidated compounds;
- (c) introducing desorbent containing sulfur-oxidated compounds from step (b) into a high sulfur, lower end zone of a split shell fractionation column;
- (d) contacting the adsorbent from step (b) with a hydrocarbonaceous stream containing sulfur-oxidated compounds;
- (e) introducing an initial portion of an effluent from step (c) comprising desorbent from step (b) into a low sulfur, lower end zone of said split shell fractionation column,
- (f) fractionating the desorbent containing sulfur-oxidated compounds from step (b) to recover a desorbent having a reduced concentration of sulfur-oxidated compounds; and
- (g) recovering a hydrocarbonaceous stream containing a reduced concentration of sulfur-oxidated compounds.

Claim 29 (previously added): The process of claim 28 wherein the hydrocarbonaceous stream containing sulfur-oxidated compounds boils in the range from about 149°C (300°F) to about 538°C (1000°F).

Claim 30 (previously added): The process of claim 28 wherein the fractionating in step (d) is conducted in a split shell fractionation zone.

Application No. 10/813,250
Reply to Advisory Action of 07/17/2008

Page 4

Claim 31 (previously added): The process of claim 28 wherein at least a portion of the desorbent having a reduced concentration of sulfur-oxidated compounds recovered in step (d) is recycled to step (b).

Claims 32-44 (canceled herein)